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(54) **PROCESS FOR TREATING WASTE WASHING WATER USED FOR IMPREGNATION.**

(57) A process for treating waste washing water, which is only slightly affected by the temperature and can dispense with any chemical and wherein the quality of treated water is not affected by a change in the waste water concentration. The process comprises conducting impregnation with an impregnant having a composition comprising triethylene glycol dimethacrylate, 2-hydroxyethyl methacrylate, lauryl methacrylate, nonionic surfactant and azobisisobutyronitrile, separating the impregnant thereafter, washing the surface of an impregnated article with water, and treating the waste water with a liquid obtained by filtering the liquid having the above composition through a filter having a retained

particle diameter of 20 μ m or less.

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[Technical Field]

This invention relates to a method for the treatment of the effluent from the washing with water of an impregnated object, which method accomplishes the treatment without specially requiring addition of a chemical agent.

[Background Art]

The practice of using a liquid impregnant such as of sodium silicate or an unsaturated polyester or an aerophobic liquid impregnant for the purpose of infallibly sealing invisible pinholes in die-cast products and cast products of aluminum, zinc, and other metals, completely filling and sealing pores in sintered metal parts, preventing plated products from blowing by subjecting the parts to the treatment of impregnation before the step of plating, and sealing minute pores in such porous non-metallic parts such as of wood and ceramics has been in vogue.

For example, the impregnation of a given part is attained by defatting and cleaning the part, subjecting the cleaned part to vacuum aspiration in a vacuum tank thereby removing entrapped air from the minute pores in the part, then immersing the part in a bath of an organic liquid impregnant such as an aerophobic resin, maintaining the part in a vacuum, and subsequently exposing the immersed part to the atmospheric pressure thereby causing the liquid impregnant to permeate the minute pores. In this case, the impregnation can be enhanced by supplying compressed air to the site of impregnation. Then, the liquid impregnant is returned to the reservoir and the part which has undergone the impregnation is centrifuged to expel the liquid impregnant adhering to the surface of the part. Thereafter, the part is cleaned with a detergent to remove the liquid impregnant still remaining on the surface of the part or in the tapped holes. The treatment of impregnation is finished by subjecting the part to the treatment for curing.

In this treatment of impregnation, the effluent to be discharged from the site of treatment is the spent detergent which occurs when the liquid impregnant remaining only slightly on the surface of the part which has undergone the treatment of impregnation is washed off with a detergent. Heretofore, such organic solvents as trichloroethane and fluorinated hydrocarbon have been used as detergents. On account of the anxiety about the environment and the concern about cost, the use of such organic detergents has been giving place to the use of water for the cleaning. In consequence of this trend, there has arisen the necessity for separating and recovering the liquid impregnant contained in the effluent before the effluent is dis-

carded from the plant. This separation of the liquid impregnant from the effluent is a difficult matter.

For the treatment of the effluent of this nature, the following methods have been available to date.

(1) Method of adsorption: The liquid impregnant which is an organic substance is removed by adsorption using an adsorbent such as activated carbon. By this treatment, both the BOD and COD contents in the effluent can be lowered to below several ppm. Thus, this method may well be called a method for final treatment productive of an effluent tolerable for release into river.

(2) Method of microorganic decomposition: This method, represented by the version resorting to the action of activated sludge, allows the same degree of treatment as the method of adsorption by the decomposition of organic matter with aerobic bacteria.

(3) Method of combustion: The effluent is dispersed in heavy oil and the resultant mixture is burnt as sprayed into a flame. Since this combustion produces carbon dioxide gas and water, this method effects perfect detoxication of the effluent.

(4) Method of thermal polymerization: This method utilizes the phenomenon that an impregnant polymerized in water is insoluble in water. Generally, the water containing the impregnant is heated for the purpose of promoting the reaction. The treated effluent is subjected to solid-liquid separation by filtration or settling (difference in specific gravity). The treated effluent has a COD content of from some thousand to some tens of thousand ppm and, therefore, is generally not allowed to be released into rivers. It is, either subjected to another final treatment or reclaimed as washing water.

(5) Method of separation by flocculation: This method, primarily intended for the removal of suspended matter from water, is capable of causing incorporation of a water-soluble liquid impregnant in the product of flocculation. The treated effluent substantially equal in quality that obtained by the method of thermal polymerization.

The methods of (1) and (2) are both classical ways of waste water disposal and may well be called as mature techniques. Their execution, however, entails a space and cost for installation of apparatus for impregnation. The exclusive use of these methods as means for impregnation is practically infeasible, with the running cost as a contributory factor. The method of combustion of (3) operates with a relatively simple apparatus and relies for treatment simply on the phenomenon of combustion and may well be called a method of popular use. The largest problem confronting this method is the fact that the vaporization of water which accounts for the best part (about 90%) of the effluent consumes a large volume of energy and the expense of fuel for the vaporization brings a huge addition to the running cost. The method of

(4) utilizes the reactivity owned by the impregnant and enjoys popular acceptance next to the method of (3). This method, however, necessitates numerous auxiliary devices such as the devices for injection of a flocculating auxiliary and a pH adjusting agent, a reaction tank, a separation tank, and a device for cooling the treated effluent, for example. Moreover, the by-product of reaction defies elucidation and control. These facts coupled with the cost of energy for heating and cooling prevent this method from being disseminated. The method of flocculation of (5) necessitates the same apparatus as the method of heating, excepting it has no use for devices used for heating and cooling. Since the floc produced by this method has low strength, the liquid impregnant contained in the floc is suffered to redisperse when the speed of filtration for separation is heightened and the load exerted on the device for filtration increases when the speed of filtration is slowed.

The conventional methods of treatment except for the method of thermal polymerization utilizing the reactivity owned by the liquid impregnant turn out to be those generally employed for the disposal of other industrial effluents. Since the polymerization hinges heavily on temperature, the method of thermal polymerization calls for a device for temperature control and a device for cooling the treated effluent for reclamation. The other conventional methods are in such a state that they do not deserve to be called as fully satisfactory measures for the treatment of the effluent emanating from the apparatus of impregnation for the reason given above. Thus, the desirability of developing a method of an entirely novel concept which provides a highly efficient and economically advantageous treatment of the effluent under discussion has been finding enthusiastic recognition.

An object of this invention is to provide a method for the treatment of the effluent from the process of detergency, which is affected by temperature only to a small the quality of which extent, requires no addition of a chemical agent, and produces a treated water is not affected by a change in the effluent concentration.

[Disclosure of Invention]

The present inventor has contained a study with a view to solving the problems mentioned above and fulfilling the object mentioned above, to find that the effluent can be adapted to undergo precision filtration for separation highly effectively by using a liquid impregnant containing a water-insoluble monomer in an increased concentration thereby converting the effluent from the solution system incorporating therein the liquid impregnant subjected to separation on the molecular level to

the dispersion system having incorporated therein from several to some hundred or more monomers associated in the form of micelles (oil drops). He has perfected this invention as a result. To be specific, this invention concerns a method for the treatment of the effluent from the washing with water of an impregnated object produced by the treatment of impregnation using an organic impregnating agent having as a main component thereof an acrylic type or methacrylic type monomer containing at least 30% of a cross-linking agent or a water-insoluble monomer, which method is characterized by effecting the treatment of the effluent by the treatment of filtration using a filter medium having an average retained particle diameter of at least 20 μm .

The effluent from the treatment of impregnation which is involved in the present invention issues from the treatment of impregnation using an organic liquid impregnant having as a main component thereof an acrylic or methacrylic type monomer containing at least 30% of a cross-linking agent or a water-insoluble monomer. As an example of the cross-linking agent, a sparingly water-soluble cross-linking agent such as triethylene glycol dimethacrylate may be cited. As examples of the water-insoluble monomer, lauryl methacrylate and slightly water-soluble 2-hydroxy methacrylate may be cited. The lower limit of 30% is fixed for the content of the cross-linking agent or the water-soluble monomer because the necessity arises for notably lowering the retained particle diameter, the material for the filter medium is restricted, and the efficiency of separation is seriously degraded when the soluble monomer is contained in a large amount. The acrylic or methacrylic type monomers which are allowable herein include trimethylol propane tri(meth)acrylates, 1,6-hexane di(meth)acrylates, neopentyl glycol di(meth)acrylates, neopentyl glycol di(meth)acrylates, polyethylene glycol di(meth)acrylates, 2-hydroxyethyl (meth)acrylates, and methoxypolyethylene glycol mono(meth)acrylates, for example.

The concentration which the effluent resulting from the treatment for impregnation using the liquid impregnant assumes at the time of treatment is altered by the regulation of the speed of filtration and, by nature, has no particularly suitable level. It may be suitably fixed in due respect of the economy and efficiency of the treatment with relation to the device used for the treatment of impregnation.

The filter medium is selected from among such substances as cellulose, tetrafluoroethylene, polysulfone, aromatic polyamides, glass fibers, alumina, and titanium dioxide which have average retained particle diameters of at least 20 μm , in due consideration of the state and degree of concentration of the effluent and the durability of the filter medium.

In terms of the resistance to chemicals, tetrafluoroethylene, glass fibers, alumina, and titanium dioxide prove to be particularly suitable. An inorganic membrane permits easy use from the viewpoint of the treatment for regeneration.

For example, alumina type filter medium is formed by boring a plurality of pores in a cylindrical support of coarse particles, wherein the inner surface of each of the pores is lined with a film of fine particles.

The upper limit of 20 μm is fixed for the average retained particle diameter because the exclusive use of the liquid impregnant suffices for the treatment of the effluent and does not entail use of a special flocculation aid. When the flocculation aid is used, it allows a further addition to the coarseness of the filter medium fit for effective use in the treatment.

Though an elevation of the temperature of the effluent during the treatment of filtration is beneficial because it proportionately lowers the viscosity of water and increases the speed of filtration, the treatment of filtration can be carried out sufficiently at normal room temperature.

The separation by filtration is a technique which has been used long for the separation of a solid from a liquid. Also in the field of waste water disposal, it is widely used in the solid-liquid separation by the method of flocculation and for the prefilter in the tank for adsorption with activated carbon. Recently, owing to the advance of the filter medium, the technique of filtration is now capable of not merely effecting separation of an oil emulsion and solid-liquid separation due to desalination but also realizing solid-liquid separation and molecular level separation.

If the liquid impregnant is set to have pH 7-8, the value of which being necessary for washing the metal, it will not be required to adjust the pH.

The fact that a water-soluble monomer can be separated by the precision filtration of this kind is theoretically understandable. In fact, a methacrylic acid type water-soluble monomer can be separated by the method of reverse osmosis filtration. The efficiency of this separation, however, does not deserve to be called fully satisfactory. When the concentration is carried out to the level of 20 to 40%, the membrane used for the filtration betrays vulnerability to chemicals and suffers from a notable decrease in service life. The solution of this problem necessitates development of a novel membrane for separation. The membrane also entails no few problems awaiting solution in terms of maintenance. The separation by the membrane, therefore, has appeared to be hardly feasible. In the development of this membrane, it has been demonstrated that the filter medium is allowed to contain pores of a large diameter and use a ma-

terial selected from a rich variety of materials by heightening the water-insoluble monomer concentration and effecting conversion of the effluent from the solution system incorporating therein the liquid impregnant for separation on the molecular level to the dispersion system having from several to some hundred or more monomers incorporated therein associated in the form of micelles (oil drops). Generally for the separation of a solution incorporating such monomers on the molecular level therein, the reverse-osmosis filtration (RO) to the ultrafiltration (UF) are partly used. For the separation of the dispersion system, the UF to the filter membrane having a retained particle diameter ranging from several μm to some tens of μm are used. The enlargement of the retained particle diameter brings about the advantage of widening the spectrum of selection of the filter medium and facilitating measures to cope with the problem of chemical resistance and maintenance. At the same time, the amount of the effluent to be filtered per unit surface area tends to increase in proportion as the diameter for filtration increases. This increase in the amount of the effluent to be filtered greatly contributes to decreasing the size of a plant.

The study on the relation with the composition of the liquid impregnant has imparted a great potentiality to the method of separation by filtration which has found a greatly limited utility. The extensive use of a water-insoluble monomer in the step devoted basically to the purification of water, however, incurs a serious drawback in terms of the ability of purification and necessitates a technique for advanced utilization of a surfactant. This technical requirement has conversely urged perfection of a technique for utilizing the surfactant in alleviating the deteriorated permeation of the monomer through the membrane for separation.

[Best Mode for Carrying Out the Invention]

Example:

An aqueous solution containing 5% of suspended matter composed of 65 parts of triethylene glycol dimethacrylate, 19.7 parts of 2-hydroxyethyl methacrylate, 10 parts of lauryl methacrylate, 5 parts of nonionic surfactant, and 0.3 part of azobisisobutyronitrile was prepared and passed through a 0.1 μm -PTFE membrane to collect the suspended matter on the membrane. The SS concentration, by determination of weight difference before and after the treatment of purification, was found to be 5992 mg/liter. The separation with a 0.1 μm alumina type filter produced a colorless, transparent liquid having a COD content of 9,700 mg/cg. This liquid was found to be fully utilizable as washing water. When this treatment was consecutively used for

one week, the filter showed a gradual decrease in the amount of water permeated therethrough and, at the end of one week's use, showed a clogging of 10%. When the filter was regenerated by burning, it resumed the initial capacity for permeation. This the regenerated filter was again usable for the treatment.

Comparative Experiment:

An aqueous solution containing 5% of suspended matter composed of 89 parts of 2-hydroxyethyl methacrylate, 10 parts of polyethylene glycol dimethacrylate, and 1 part of benzoyl peroxide and passed through a 0.1 μ m-PTFE membrane to collect the suspended matter on the membrane. The SS concentration, by determination of the weight difference before and after the treatment for purification, was found to be nil.

[Industrial Applicability]

This invention consists in filtering with a filter medium having a specific average retained particle diameter the effluent from the treatment for impregnation using a liquid impregnant containing a cross-linking agent for a water-insoluble monomer in a specific concentration. This filtration, therefore, yields only slightly to the effects of concentration and temperature of the effluent, obviates the necessity for adding any special chemical agent, finds no use for a large space and high expenses of equipment and fuel which have been inevitable for the conventional treatment of effluent by impregnation, allows easy control of operation, and permits the treatment to be carried out inexpensively and infallibly. Thus, the present invention proves to be highly effective.

Claims

1. A method for the treatment of the effluent from the washing with water of an impregnated object produced by the treatment of impregnation using an organic impregnating agent having as a main component thereof an acrylic type or methacrylic type monomer containing at least 30% of a cross-linking agent or a water-insoluble monomer, which method is characterized by effecting said treatment of the effluent by the treatment of filtration using a filter medium having an average retained particle diameter of at least 20 μ m.
2. The method as claimed in claim 1, wherein the cross-linking agent is a water-insoluble cross-linking agent.

3. The method as claimed in claim 1, wherein the filter medium is any one selected from the group consisting of cellulose, tetrafluoroethylene, polysulfone, aromatic polyamides, glass fiber, alumina and titanium dioxide.

INTERNATIONAL SEARCH REPORT

International Application No. PCT/JP92/00380

I. CLASSIFICATION OF SUBJECT MATTER (If several classification symbols apply, indicate all) *		
According to International Patent Classification (IPC) or to both National Classification and IPC		
Int. Cl. ⁵ C02F1/44, B01D61/14, 37/00		
II. FIELDS SEARCHED		
Minimum Documentation Searched *		
Classification System	Classification Symbols	
IPC	C02F1/44, 1/52, B01D61/14, 37/00, 37/06	
Documentation Searched other than Minimum Documentation to the Extent that such Documents are Included in the Fields Searched *		
Jitsuyo Shinan Koho		1926 - 1991
Kokai Jitsuyo Shinan Koho		1971 - 1991
III. DOCUMENTS CONSIDERED TO BE RELEVANT *		
Category *	Citation of Document, ** with indication, where appropriate, of the relevant passages **	Relevant to Claim No. **
X	JP, A, 57-177305 (Sumitomo Chemical Co., Ltd.), November 1, 1982 (01. 11. 82), Claim, lines 4 to 6, lower left column, page 2 (Family: none)	1-3
A	JP, A, 52-152658 (Dai Nippon Toryo Co., Ltd.), December 19, 1977 (19. 12. 77), (Family: none)	1-3
A	JP, A, 55-8824 (Tosoh Corp.), January 22, 1980 (22. 01. 80), Lines 5 to 7, upper right column and lines 11 to 14, lower right column, page 3, example 2 (Family: none)	1-3
A	JP, A, 54-44609 (Nippon Shokubai Kagaku Kogyo Co., Ltd.), April 9, 1979 (09. 04. 79), (Family: none)	1-3
<p>* Special categories of cited documents: **</p> <p>"A" document defining the general state of the art which is not considered to be of particular relevance</p> <p>"E" earlier document but published on or after the international filing date</p> <p>"L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)</p> <p>"O" document referring to an oral disclosure, use, exhibition or other means</p> <p>"P" document published prior to the international filing date but later than the priority date claimed</p> <p>"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention</p> <p>"X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step</p> <p>"Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art</p> <p>"S" document member of the same patent family</p>		
IV. CERTIFICATION		
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June 16, 1992 (16. 06. 92)		July 7, 1992 (07. 07. 92)
International Searching Authority		Signature of Authorized Officer
Japanese Patent Office		